

Proper Pump Installation Practices





There is a Reason Every Unit Comes With This Bright Orange Tag !

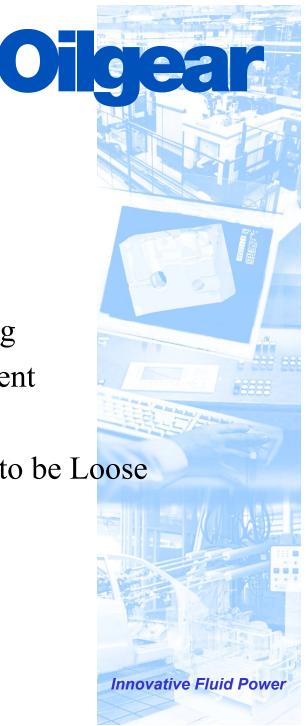






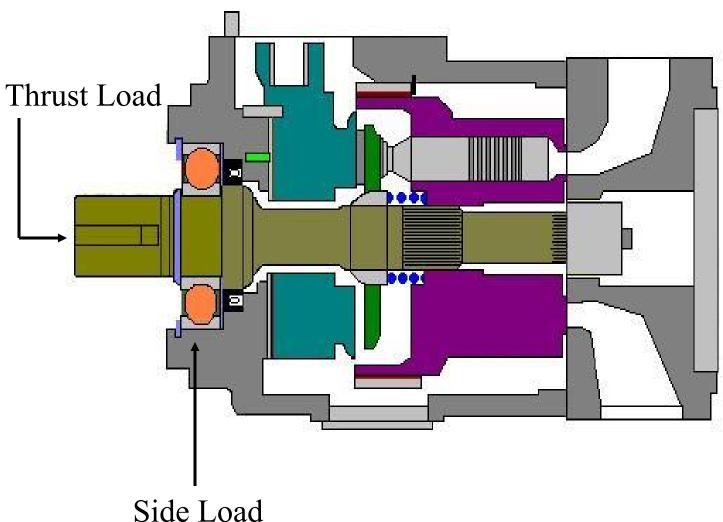
Proper Alignment and Coupling Installation

- Do Not Drive Coupling Onto Shaft
- Pump Alignment Must be .005" TIR
- Make Sure Coupling Halves are Not Touching
 *Can Induce Thrust load and Misalignment
- Use Keyed Shaft for Industrial Applications
 *Oilgear Standard Splines are Designed to be Loose
 *Do Not Use Split Spline Couplings

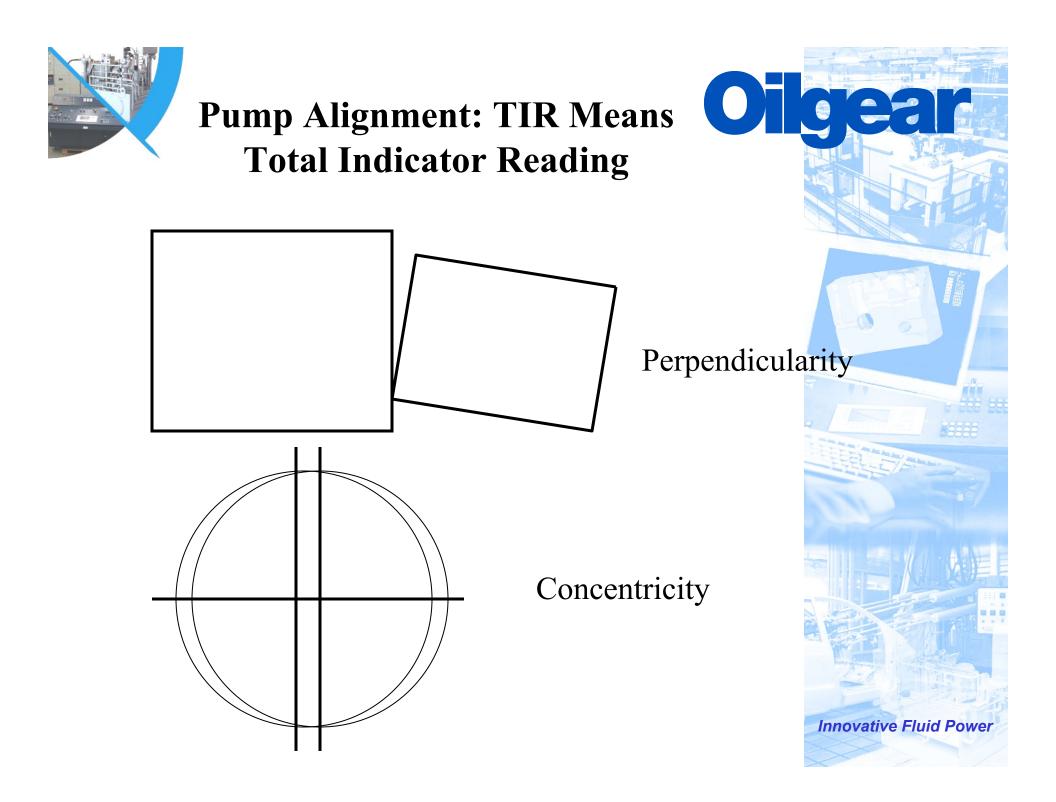


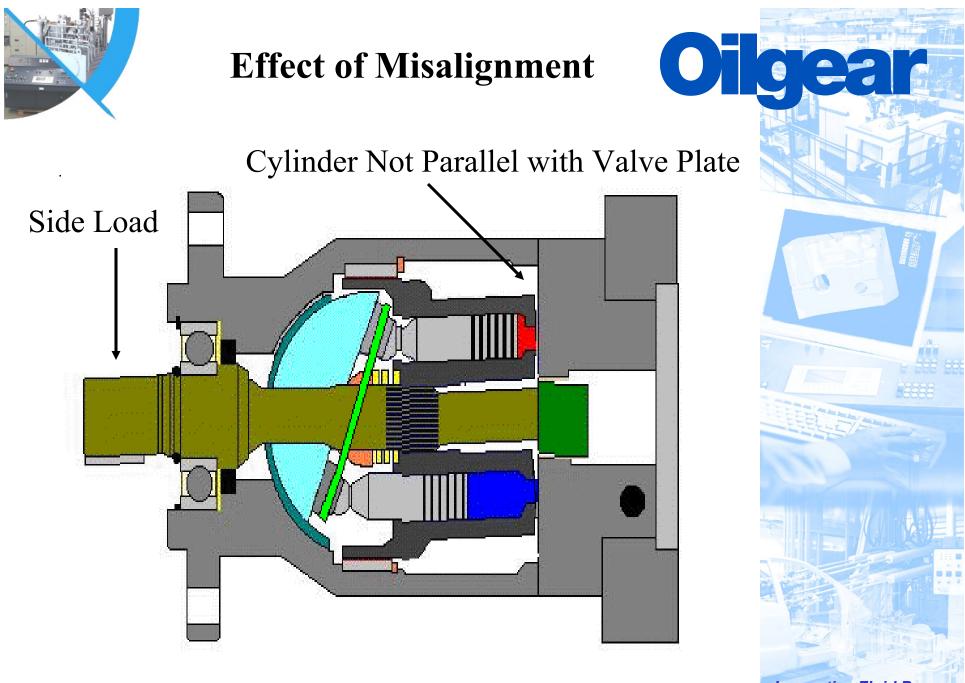


Bearings are Designed to Carry Oligonia Side Loads Not Thrust Loads



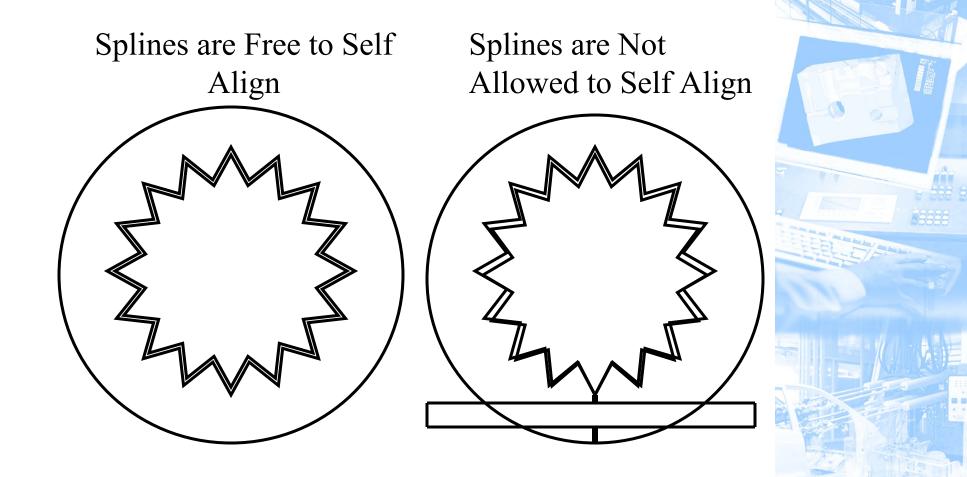
Driving on a coupling or coupling halves touching -Creates a thrust load, damaging balls and race's of front bearing.







Split Couplings Can Cause Misalignment



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Case Drain Lines

• Lines Must be Full Size

Lines

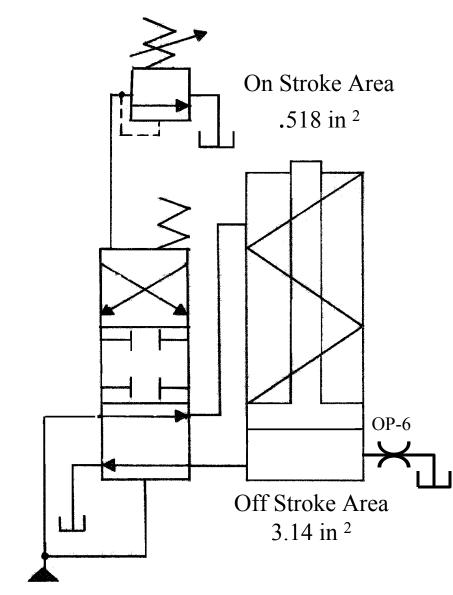
• Lines Must be Unrestricted

 \mathbf{O} Lines May Not be Connected to Other Return

- Lines May Not be Connected to Filters, Coolers Lines Must be Plumbed so that Case Remains Full at All Times
- Lines Must be Terminated Below Oil Level



Case Slip Increases When Unit Strokes



PVG "C" Frame Stroke = .750" On Stroke Response = 40 ms Off Stroke Response = 50 ms Amount of Flow Being Drained to Case On Stroke = 15.16 GPM Off Stroke = 2.018 GPM Add in Pump Leakage Full Stroke Leakage, On Stroke = 4 GPM Compensated Leakage, Off Stroke = 7 GPM

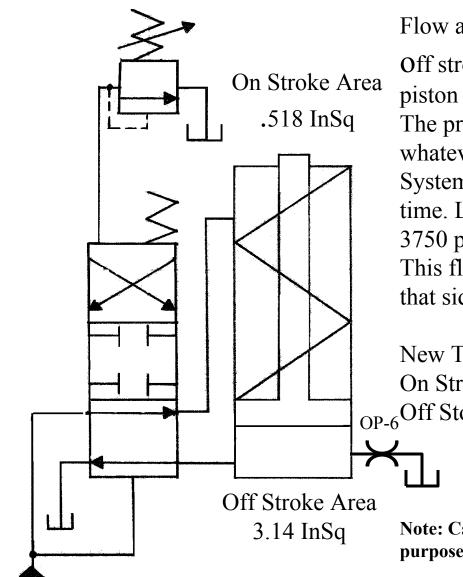
Total amount of flow that must be accelerated through case drain line.

On Stroke = 19 GPM Off Stroke = 9.018 GPM

Note: Calculations on this slide are for visual illustration purpose's only.



Case Slip Increases When Unit Strokes Continued



Flow across OP-6 must be added in when going

Off stroke. When oil is ported to off stroke side of piston it also bleeds to tank through this orifice. The pressure on that side of the piston will go to whatever it needs to in order to move the piston. System pressure could be seen for a short period of time. Let's use 3750 psi -3750 psi across .081" dia orifice = About 11 GPM. This flow is not added in when going on stroke as that side of the piston is open to tank.

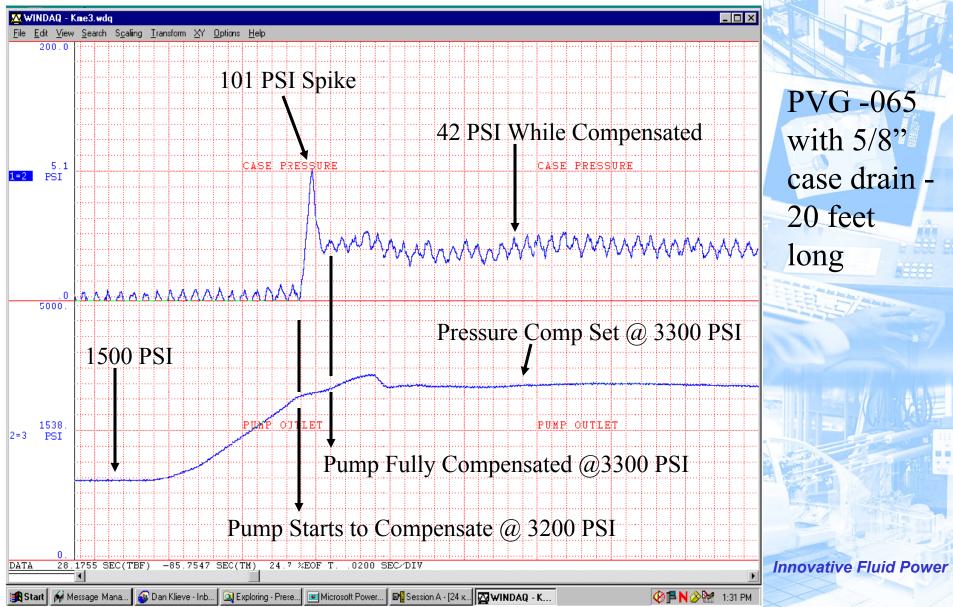
New Totals On Stroke = 19 GPM $_{OP-6}Off$ Stoke = 20.018

20 GPM Has to be Accelerated Through Case Drain Line When Pump Shifts

Note: Calculations on this slide are for visual illustration purpose's only.



Case Spike While Pump Comes Off Stroke

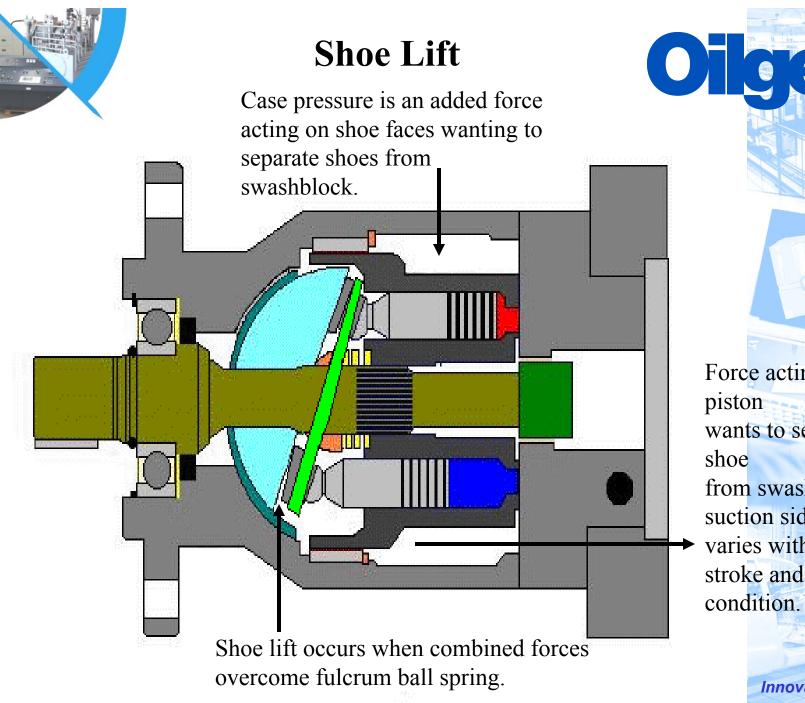




Effects of Case Pressure

- Shaft Seal Failure
 - *Standard Seal Rated to 25 PSI
- Gasket Failures
- Piston Shoe Swashblock Failure
 *Shoe Lift



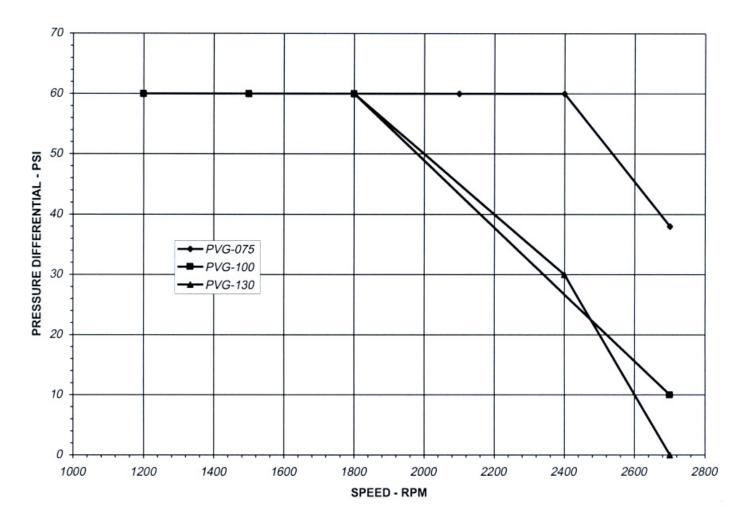


Force acting on wants to separate from swashblock on suction side, force varies with rpm, stroke and inlet



Shoe Lift Occurs Due to Case to Inlet Differential Limits

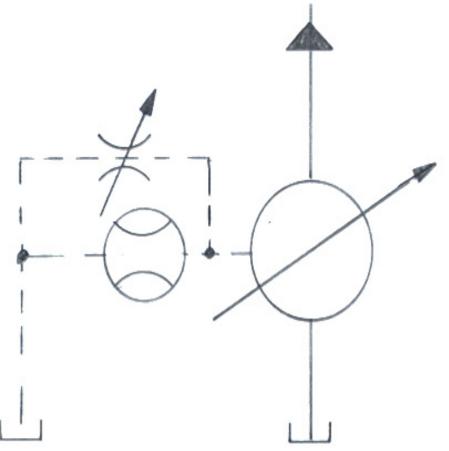
MAXIMUM CASE/INLET PRESSURE DIFFERENTIAL



tive Fluid Power



Flow Meter in Case Drain Line Not Recommended, But if You Must



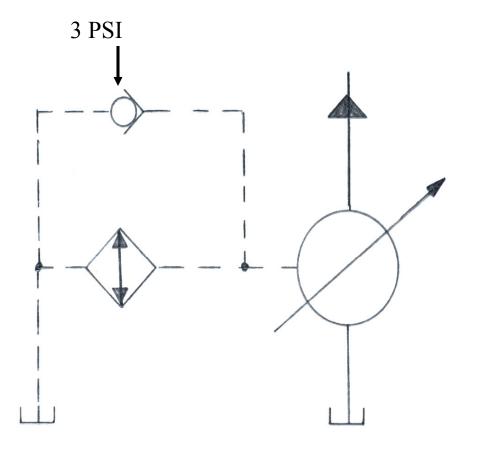
Put a full size ball valve in parallel with the meter. Ball valve should be **open** during **Normal Operation**. Close the valve to check case slip when needed. This does 2 things:

1) It Protects the Pump From Case Spikes.

2) It Saves Wear and Tear on the Meter When the Pump is Cycling



Cooler in Case Drain Line Not OF Recommended, But if You Must



Put a 3 PSI check valve in parallel with cooler to protect pump from case spikes.





Inlet Conditions

- Inlet Lines Should be Full Size
- Inlet Lines Should be Unrestricted and as Short as Possible
- Inlet Lines Should Have a Minimum of Fittings and Elbows
- Inlet Location
 - *Away From Return Lines
 - *Proper Reservoir Baffling
- Suction Strainers are Not Recommended
 *If Required Size for 3 Times Pump Volume





Inlet Sizing on Variable



Displacement Pumps is Critical

PRESSURE REQUIRED @ PVG-130 INLET STEADY STATE MIN. INLET REQUIRMENT 1800 RPM = 11 PSIA LOSS THROUGH 2.5" PIPE WITH ONE ELBOW = APPROXIMATIVELY .3 PSI

PRESSURE @ THE INLET @ SEA LEVEL 14.4 PSIA

PRESSURE REQUIERED WHILE COMING ON STROKE @ 50 MS SAME LOSS DUE TO PRESSURE DROP = .3 PSIA ADDED LOSS DUE TO ACCELERATING THE COLUMN OF FLUID IN 50 MS = 2.46 PSIA

PRESSURE @ THE INLET WHILE PUMP COMES ON STROKE IN 50 MS @ SEA LEVEL = 11.9 PSIA

The above is under best of circumstances on oil. Even with that we are approaching the cavitation point of the pump. Many things contribute to inlet requirement, such as Fluid Type, Line Length, Any Inlet Restrictions, RPM, Elevation.



Inlet Sizing on Variable

Displacement Pumps is Critical

IF THE HIGH RESPONSE TIME IS NOT REQUIRED YOU CAN MAKE THIS CONDITION BETTER

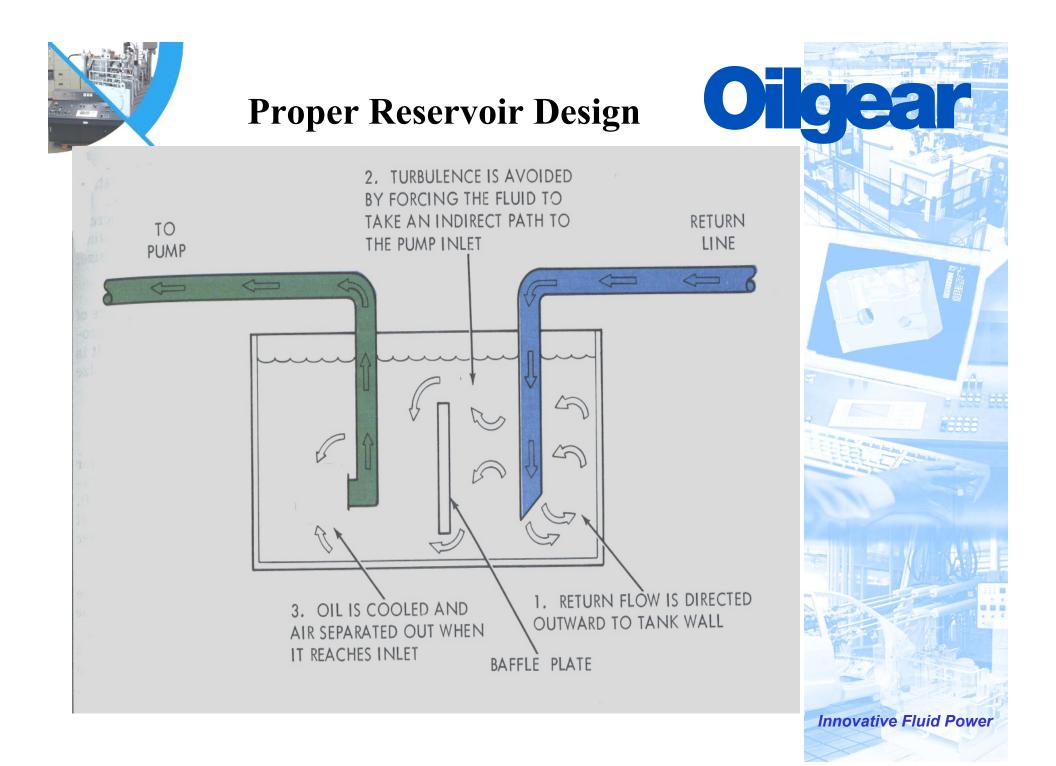
PVG-130 WITH RESPONSE SLOWED TO 200 MS

SAME LOSS DUE TO PRESSURE DROP = .3 PSIA ADDED LOSS DUE TO ACCELERATING THE COLUMN OF FLUID IN

200 MS = .7 PSIA

PRESSURE @ INLET WHEN PUMP COMES ON STROKE IN 200 MS @ SEA LEVEL = 13.5 PSIA

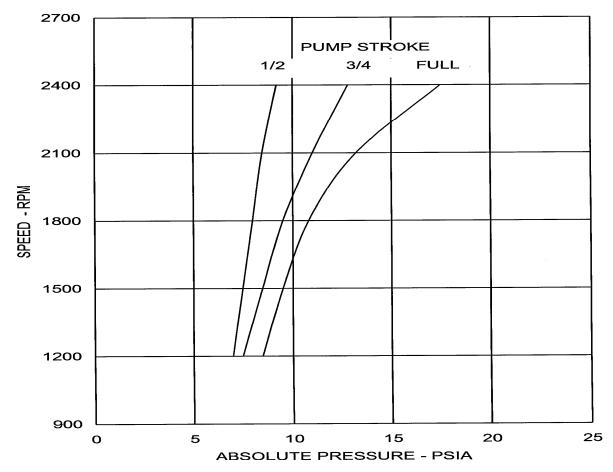
This condition allows a little more room for other added losses such has Heavier Fluids, Longer Line Lengths, Higher RPM, Elevation.





Be Aware of Pump Inlet Characteristics

PVG-130 SUCTION TEST



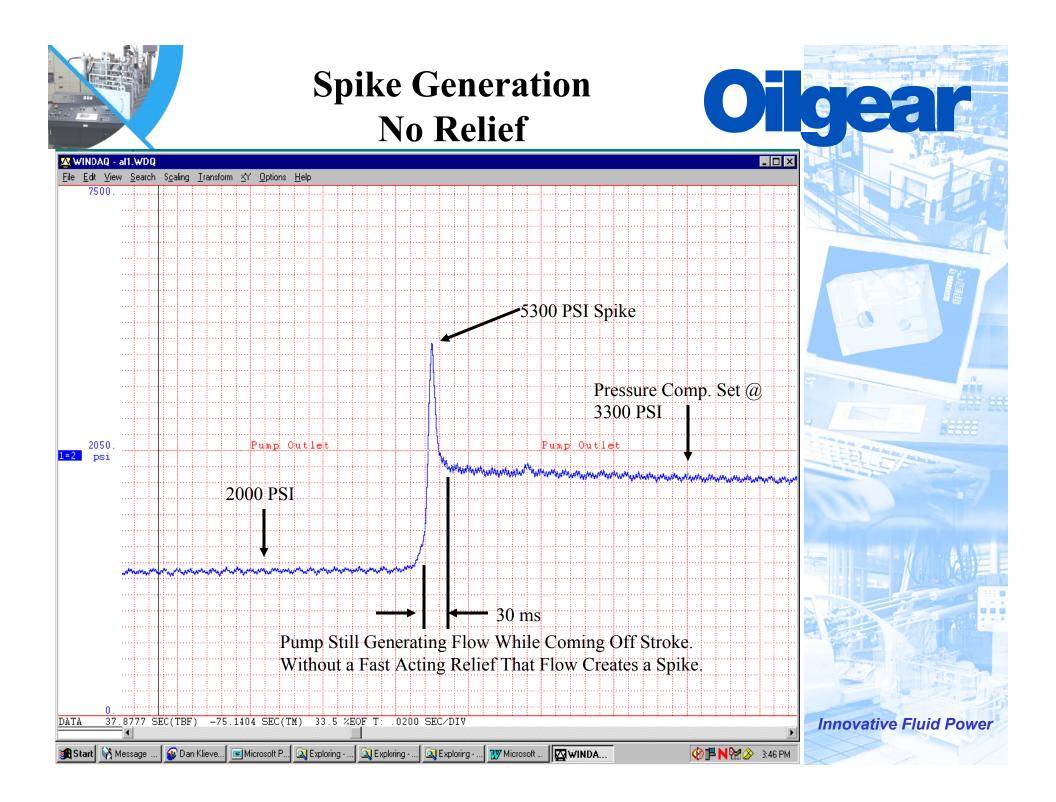
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Fast Acting Relief

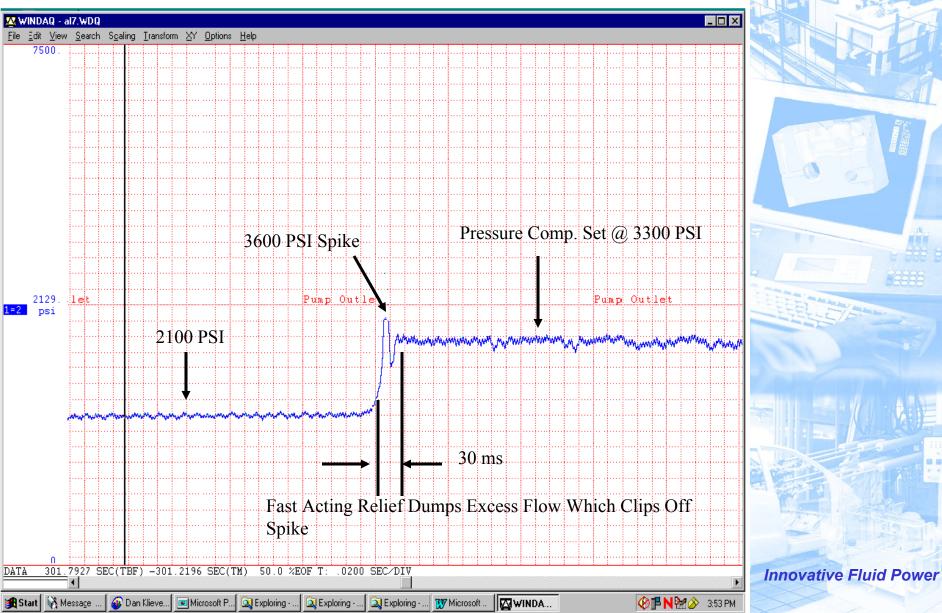
- Fast Acting Relief Always Recommended
- Pressure Compensators Not Meant to Act as System Relief
 - *Flow is Still Being Delivered to the System While Pump is Coming Off Stroke
- Relief Should be Set 300 PSI Above Compensator Setting







Spike Generation With Relief





Filtration

- Use Minimum 10 Micron Filters
- Use By-Pass Filters With Indicators
- Off Line Filtration Preferred
- Keep Fluid to Recommended ISO Level





Start Up



- Make Sure Tank is Full of Fluid
- Make Sure All Shut off Valves are Open
- Fill Case Completely Before Operating
- Check for Proper Rotation
 *Rotation is Referenced Looking at Pump Shaft
- Provide a Means of Purging Air From Discharge Line
- Back Out Pressure Compensator and System Relief
- Jog Motor if Possible



• Following the proper installation procedure directly relates to the success of the application and the life of the pump.

Thank-You



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